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BOX PATENT APPLICATION
Assistant Commissioner for Patents
Washington, D.C. 20231

NEW APPLICATION TRANSMITTAL

Transmitted herewith for filing is the patent application of:

Inventor(s): Kevin M. McHugh

For (title): Rapid Solidification Processing System for Producing Molds, Dies and Related Tooling

Enclosed are:

- ☒ 8 sheets of drawing(s). ☐ informal ☐ formal
☒ An assignment of the invention to Bechtel BWTX Idaho, LLC
☐ A certified copy of a _____ application.
☐ An associate power of attorney.
☒ Combined Declaration and Power of Attorney.
☐ Information Disclosure Statement.
☐ Form PTO-1449 (together with citations).

Fee Calculation (37 CFR 1.16)

CLAIMS AS FILED

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Multiple dependent claim(s), if any (37 CFR 1.16(d))		\$260.00	= 0
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BOX PATENT APPLICATION
Assistant Commissioner for Patents
Washington, D.C. 20231

EGG-PI-612A1a, "RAPID SOLIDIFICATION PROCESSING SYSTEM FOR PRODUCING
MOLDS, DIES AND RELATED TOOLING"

Dear Sir:

Enclosed is the subject patent application, 8 sheets of drawings, together with an executed
Combined Declaration and Power of Attorney; a Patent Assignment, together with a Recordation
Form Cover Sheet; a fee sheet, in duplicate; and a return receipt postcard.

Sincerely,

Patricia A. Butikofer
Intellectual Property Administrator
Technology Transfer Office

PB

Enclosures

cc: R. J. Fisher, DOE-CH (w/o Encl)

Express Mail #EI568915941US

Atty. Dkt. No.: EGG-PI-612A1a

**Title: RAPID SOLIDIFICATION PROCESSING SYSTEM FOR PRODUCING
MOLDS, DIES AND RELATED TOOLING**

Inventors: Kevin M. McHugh

EGG-PI-612A1a

1 **RAPID SOLIDIFICATION PROCESSING SYSTEM FOR PRODUCING**
2 **MOLDS, DIES AND RELATED TOOLING**
3

4 This is a continuation of United States application S/N 09/023,037 filed
5 February 12, 1998, now U.S. Patent No. _____ which is hereby incorporated by
6 reference.
7

8 **CONTRACTUAL ORIGIN OF THE INVENTION**

9 This invention was made with United States Government support under Contract
10 No. DE-AC07-94ID13223, now Contract No. DE-AC07-99ID13727 awarded by the
11 United States Department of Energy. The United States Government has certain rights in
12 the invention.
13

14 **BACKGROUND OF THE INVENTION**

15 This invention relates to a method for the production of dies and molds and more
16 particularly to a spray forming process for the deposition and rapid solidification of
17 atomized molten droplets onto a pattern for manufacturing dies, molds and related
18 tooling.

19 The recent explosion of interest in rapid prototyping technology is fueled in part
20 by the restructuring of today's marketplace. Successful competition in global markets
21 will require the ability to carry a design concept through the prototype stage to the
22 production stage faster and at lower cost than ever before. The ability to generate plastic

1 and wax models of prototype parts with high dimensional accuracy via selective laser
2 sintering, stereolithography, and other approaches is now a reality. The rapid production
3 of prototype parts from engineered materials (i.e., materials that will actually see service)
4 is a prime goal of industry. Methodologies that can rapidly produce specialized tooling,
5 such as molds and dies, would satisfy this goal when used with conventional
6 manufacturing techniques such as injection molding, blow molding, compression
7 molding, stamping and die casting.

8 Presently, complex molds, dies and related tooling produced by conventional
9 machining methods are expensive and time consuming to make. Costs can easily exceed
10 hundreds of thousands of dollars and fabrication can require months of effort to produce
11 molds with highly accurate dimensions and tolerances within a few mils or less.

12 As a consequence of the various disadvantages of conventional machining
13 methods, thermal spray forming processes have been developed for fabricating dies
14 whereby a deposition of a metallic layer on a plaster or metal casting is used to produce
15 the die shell. These conventional processes utilize wire or powder feedstocks and are
16 currently limited to a maximum spray rate of approximately 15 grams per second.

17 Conventional thermal spray processes produce relatively large droplets, generally with
18 mass median diameters in the order of magnitude of 100 μm and with a rather broad
19 distribution of droplet size. Due to the large droplet size, low deposition rate, and heat
20 content associated with conventional spray processes, solidification of the deposited
21 droplets results in relatively poor microstructure, poor mechanical properties, porous
22 deposits and limited material choices. Most high strength metals, including low-carbon,

1 tool, hardfacing and stainless steels have high melting temperatures, thereby limiting the
2 choice of materials used for the pattern or requiring a protective coating on the pattern to
3 protect the pattern from the high temperature metal if conventional spray techniques are
4 to be used. Conventional thermal spray techniques also require feedstocks in the form of
5 metal powders or wires which are relatively expensive and limit material choices.

6 It is therefore an object of this invention to provide an improved spray forming
7 system for the manufacture of molds, dies and related tooling by controlling the in-flight
8 cooling of atomized droplets, thereby controlling the temperature and solidification of the
9 droplets that are deposited on a pattern..

10 It is another object of this invention to provide a spray forming system for the
11 manufacture of molds, dies and related tooling by controlling the temperature and
12 composition of a quench gas contained within a chamber through which the atomized
13 droplets are directed.

14 Additional objects, advantages and novel features of the invention will become
15 apparent to those skilled in the art upon examination of the following and by practice of
16 the invention.

17 18 **SUMMARY OF THE INVENTION**

19 To achieve the foregoing and other objects, the spray forming system of the
20 present invention provides a method for manufacturing net shape molds, dies and other
21 tooling with excellent pattern surface finish replication by controlling the deposition
22 conditions of droplet size, velocity, heat content, flux and flow pattern. It is also

1 understood that the quality of the spray formed mold, die, or other tool reflects the
2 interplay of the above mentioned properties of the spray (e.g., droplet size, velocity,
3 liquid fraction, etc.) with the properties of the substrate (e.g., surface finish and
4 smoothness, temperature, thermal diffusivity and thermal conductivity). Polymers are
5 ideal to use as patterns for spray forming because they conduct heat very poorly and can
6 be made into complex shapes with excellent surface finish. Polymers are limited
7 however, by their maximum use temperature which is lower than many other pattern
8 materials such as ceramics. Incoming metal droplets remain fluid longer, which in turn
9 allows them to fuse together and better replicate the surface of the pattern. These
10 conditions are dependent upon the relative thermophysical properties of the sprayed
11 liquid, such as surface tension, density and viscosity, as well as the heat content and solid
12 fraction of the atomized droplets. Droplets which form the initial layer of deposit must
13 conform to the surface of the pattern in a controlled manner and solidify rapidly. Only
14 small, highly undercooled droplets or droplets with low solid fraction can meet both
15 criteria and can be produced by the technique of the present invention. A high deposition
16 rate of these droplets helps to ensure a highly dense deposit.

17 In accordance with the spray forming technique of the present application, a
18 system is provided whereby a liquid is fed or aspirated into a nozzle, through which is
19 flowing a high temperature, high velocity gas. The liquid can be any material in liquid
20 form, preferably however, the liquid is a molten metal or metallic alloy, or a polymer in
21 solution or molten form. The gas atomizes the liquid into fine droplets which are then
22 directed toward the pattern to be replicated. The atomized droplets are generally

1 spherical and of a uniform size, typically approximately less than 50 microns. The small,
2 uniform size of the atomized droplets permits an excellent replication of the pattern
3 which is evidenced, for example, by the similarity in surface roughness of the deposit and
4 pattern. The amount of heat transferred to the pattern is much less than that of the molten
5 metal starting material due to the high convection cooling rates in the spray and at the
6 pattern. The atomized droplets are rapidly quenched while still in-flight toward the
7 pattern. This is accomplished by convection heat transfer to relatively cold gas within a
8 spray chamber being entrained by the spray jet. Entrainment provides a heat sink for
9 cooling atomized droplets, thereby allowing undercooled and partially solidified droplets
10 to be formed in-flight. To rapidly quench the in-flight atomized droplets, the spray plume
11 can be directed through a quenching gas having controlled temperature and composition.
12 To further enhance the quench rate of the atomized droplets, the quenching gas can
13 initially be in the form of a cryogenic liquid, which when it comes into contact with the
14 spray jet becomes a gas. The quenching gas can be nitrogen, helium, argon, oxygen or
15 air, or any combination of these gases.

16 Analysis of the spray formed deposit also indicates the deposited material is close
17 to theoretical density, and has excellent mechanical properties. The present system is
18 capable of spraying aerosols containing solid particles which are intermixed with the
19 atomized droplets. By spraying the particles with the atomized droplets, a composite
20 mold is formed. The composite mold formed can be a metal or polymer matrix
21 composite.

1 In another embodiment of the invention, more than one kind of liquid material can
2 be sprayed. This is accomplished by having more than one controlled feed into the
3 nozzle, or alternatively, by having more than one nozzle. The separate liquids are each
4 atomized and co-deposited onto the pattern to produce functionally gradient deposits
5 and/or clad deposits.

6 7 **BRIEF DESCRIPTION OF THE DRAWINGS**

8 The present invention is illustrated in the accompanying drawings where:

9 FIG. 1 is a sectional illustration showing a preferred embodiment of the spray
10 forming device of the present application;

11 FIG. 2 is a sectional illustration of an alternate embodiment of the present
12 invention wherein an aerosol containing solid particles is utilized.

13 FIG. 3 is a sectional illustration of an alternate embodiment of the spray forming
14 device of the present application.

15 FIG. 4 is a graph showing the rapidly cooling gas temperature of the spray jet
16 after exiting the nozzle as a function of distance from the nozzle.

17 FIG.s 4A, 4B and 4C show the geometrical parameters and experimental data
18 used to generate the graph of FIG. 4.

19 FIG. 5 is a sectional illustration showing the spray forming system of the
20 present application.

21 FIG. 6 is a histogram plot showing the count frequency distribution versus powder
22 size of tin sprayed according to the method of the present invention.

1 FIG. 7 is a histogram plot showing the mass frequency distribution versus powder
2 size of tin sprayed according to the method of the present invention.

3
4 **DETAILED DESCRIPTION OF THE INVENTION**

5 Referring now to the drawings in which like numerals represent like elements
6 throughout the several views, the preferred embodiment of the present invention will be
7 described. FIG. 1 shows the spray forming device 10 of the present invention. The
8 device 10 comprises a spray nozzle 12 having a gas inlet 14 portion which converges to a
9 choke portion 16 and then diverges outwardly to an exit portion 18. Preferably the nozzle
10 is a linear nozzle (i.e. vertical plane of symmetry down the center of the nozzle along its
11 length) having a converging geometry (i.e., a nozzle flow channel which converges from
12 its inlet end to a choke portion located at the nozzle's outlet end) or a
13 converging/diverging (de Laval) geometry or is designed pursuant to the method of U.S.
14 Patent No. 4,919,853 of Alvarez et al. The temperature of the gas, sprayed liquid and
15 nozzle are controlled independently. Conventional heating methods such as resistance
16 heating, induction heating, electron bombardment heating and others are applicable. The
17 temperature of the gas entering the nozzle is controlled by a gas heater 20 connected to
18 the nozzle. Preferably the temperature of the atomizing gas entering the nozzle is in the
19 range 20 °C to 2000 °C. It is important to maintain a nozzle temperature high enough to
20 prevent the sprayed material from freezing before it is atomized. Therefore, heating
21 elements 21 for the nozzle are provided.

1 A feed assembly 22 is positioned so that the liquid is fed or aspirated near the
2 choke portion of the nozzle from the liquid reservoir 24. However, in alternate
3 embodiments of this invention, the liquid is pressure fed or aspirated through a conduit 38
4 ending proximate to the flow channel longitudinal axis at locations other than near the
5 choke portion. For example, the liquid may be fed between the flow channel inlet and the
6 choke portion or between the choke portion and the flow channel outlet end.

7 An inert atmosphere within the reservoir can be provided through a gas inlet 26
8 which also is used to provide a positive pressure within the reservoir. The inert
9 atmosphere limits the detrimental effects of atmospheric contamination. By providing a
10 pressurized liquid feed, increased atomizing gas pressure through the nozzle can be used
11 and larger throughputs of liquid material are possible. Another major advantage of using
12 a pressurized liquid feed is that it provides greater control of the operating characteristics
13 (i.e., temperature, velocity, droplet size, droplet size distribution) over conventional
14 techniques.

15 In order to maintain proper temperature control of the liquid material, the
16 reservoir is heated by heating elements 25. A thermocouple 28 measures the temperature
17 of the liquid material within the reservoir. The flow of liquid from the reservoir to the
18 nozzle is controlled by use of a stopper rod 30, whose position also provides partial
19 control of the liquid feed rate. Flow of the liquid from the reservoir is also controlled by
20 the nozzle gas flow rate (nozzle pressure).

21 Preferably the gases used are compatible with the material being sprayed and
22 generally include gases, such as argon, nitrogen, helium, air, oxygen and neon, which do

1 not react with the liquid being sprayed or with components of the spray apparatus.

2 However, in some cases it is desirable to use an atomizing gas which may react with the
3 sprayed material in a predesigned, way to improve the properties of the sprayed material.

4 For example, atomizing low carbon steel alloyed with aluminum, with nitrogen gas
5 results in the formation of fine aluminum nitride particles that act as grain boundary
6 pinning sites to refine the steel's microstructure.

7 The liquid is fed or aspirated through one or more orifices into the nozzle which is
8 transporting a high temperature gas at flow velocities ranging from high subsonic through
9 supersonic velocities. Preferably, a flow velocity is used which provides satisfactory
10 atomization of the liquid while minimizing gas usage. Also, preferably the pressure of
11 the atomizing gas at the flow channel inlet is in the range of between 100 kPa to 700kPa.
12 The gas disintegrates the liquid and entrains the resultant droplets in a highly directed two
13 phase (or multiphase) flow. During gas atomization, a liquid is disintegrated into
14 relatively fine droplets by the action of aerodynamic forces that overcome surface tension
15 forces which consolidate the liquid. The liquid's viscosity and density also influence
16 atomization behavior, but typically play a more secondary role. Viscosity affects both the
17 degree of atomization and the spray pattern by influencing the amount of interfacial
18 contact area between the liquid and gas. Viscous liquids oppose change in geometry
19 more efficiently than low viscosity liquids, making the generation of a uniform spray jet
20 more difficult for a given set of flow conditions. The density of the liquid influences how
21 the liquid responds to momentum transfer from the gas. Light liquids accelerate more

1 rapidly in the gas jet. Disintegration efficiency is reduced because atomization takes
2 place at lower relative velocities.

3 The atomized liquid droplets are directed to a pattern 34 upon which a deposit 36
4 of the rapidly cooled sprayed material is formed. Means can be provided for the relative
5 movement between the pattern 34 and the spray forming device 10 (e.g., pattern
6 manipulator 35 of FIG. 5). Using the spray forming device of the present application
7 permits a wide selection of pattern materials. For example, the pattern may be made from
8 such material as a glass, clay, wax, polymers, woods, metals, ceramics, paper. Materials
9 that are easily shaped, provide a smooth surface finish, and can withstand the temperature
10 of the spray without failure, are particularly useful with the present invention because the
11 fine and uniform size of the droplets sprayed according to the system of the present
12 invention are able to replicate fine surface detail and surface roughness of the pattern.
13 Patterns produced using rapid prototyping (solid free form fabrication) methods such as
14 stereolithography, selective laser sintering, fused deposition modeling, laminated object
15 manufacturing, etc., are very useful because they allow patterns to be produced rapidly.
16 Materials currently used by these methods can be used directly as tool patterns with low
17 melting point alloys such as tin-base or zinc-base alloys or can be used to cast a ceramic
18 or plaster tool pattern for use with high melting point alloys such as tool steels.

19 Materials capable of being sprayed by the spray forming technique of the present
20 application include, pure molten metals (such as aluminum, zinc or copper, for example),
21 metal alloys including tin alloys, aluminum alloys, zinc alloys, copper alloys, steel,
22 bronze, brass, stainless steel, tool steel and others.

1 Liquid metals are characterized by moderately high viscosity, high density, and
2 very high surface tension compared to common liquids such as methanol, water, and
3 acetone. These properties and the intrinsic high temperature requirements, make the
4 atomization of liquid metals more difficult than with most liquids. As a result, liquid
5 metal spray forming nozzles need to be designed to provide good gas/metal coupling with
6 efficient kinetic energy transfer from the gas to the metal. In linear de Laval nozzles used
7 in the method of the present invention, the liquid metal enters the flow channel with a
8 small axial velocity. There it contacts a high velocity, high temperature inert gas. High
9 temperature gas is used to help maintain the liquid metal in a fluid state throughout
10 breakup as well as to help prevent the liquid metal from freezing as it enters the gas flow
11 channel. Relatively large droplets or sheets form initially, which then undergo secondary
12 atomization by various mechanisms depending upon local flow patterns, flow velocity,
13 mass loading and the physical properties of the gas and liquid metal.

14 The dynamics of droplet breakup in high velocity flows is quite complex.
15 Historically, the Weber number (We) has been a useful predictor of breakup tendency.
16 The Weber number is the ratio of inertial forces to surface tension forces and is
17 represented by the following equation:

$$We = \frac{\rho V^2 D}{2\sigma}$$

18 where ρ is the density of the gas, V is the initial relative velocity between the flow field
19 and the droplet, D is the initial diameter of the droplet, and σ is the surface tension of the
20 droplet. Breakup of liquid droplets will not occur unless the Weber number exceeds a

critical value. Upon exiting the nozzle, the two phase (or multiphase) flow entrains relatively cold ambient gas. Examples of ambient gases capable of being utilized in the subject invention include nitrogen, argon, air, oxygen and any combinations thereof. This provides a heat sink for the atomized droplets, producing droplet populations in undercooled, liquid, solid and semi-solid states. As used throughout this application, the term "undercooling" is understood to mean cooling below the temperature at which an equilibrium phase transformation can take place without actually obtaining the transformation. Undercooling in atomized droplets involves the postponement of nucleation phenomena and is enhanced as droplet size decreases and cooling rate increases. At some point, the heat release rate within the droplet due to the liberation of the latent heat of transformation from all the nucleation sites becomes larger than the heat transfer rate to the environment, and the temperature of the droplet rises. Multiple nozzles, or multiple feed ports on a single nozzle can be used for codepositing more than one metal, ceramic or polymer.

As shown in FIG. 2, aerosols containing solid particles 23 can also be fed into the nozzle through feed line 27 and sprayed with a molten metal or polymer when spray forming particulate reinforced metal or polymer matrix composites. For example, metal matrix composites such as aluminum metal reinforced with silicon carbide particulate or fibers, can be spray formed by the technique of the present invention. A second feed port is used to introduce the ceramic material. The reinforcement phase is fed into the nozzle in the form of an aerosol upstream of the entry location of the molten metal. The particulate enters the nozzle at or near room temperature, but is quickly heated by the

1 atomizing gas to the desired temperature. The liquid metal is heated above its liquidus
2 temperature, is aspirated or pressure fed into the nozzle, atomized and codeposited with
3 the reinforcement phase. Gas and liquid metal temperature control allows control of the
4 extent of matrix/particulate wetting and interfacial reactions. The transit time of the
5 multiphase flow to the substrate is on the order of milliseconds, with droplet cooling rates
6 greater than 10^3 K/sec. Upon impacting the substrate matrix, solidification rates are
7 expected to be high, significantly restricting macrosegregation effects which are often
8 observed in slowly cooled cast composites. This approach therefore largely bypasses two
9 major problem areas experienced in most particulate reinforced metal matrix composites
10 fabrication methods -- control of matrix/particulate interfacial reactions and wetting, and
11 nonuniform blending caused by density differences between the matrix and reinforcement
12 phases. For some combinations of metal and ceramic, the ceramic particulate can be
13 added to the crucible and fed into the nozzle through the same feedport. This approach
14 requires that the metal and ceramic not react in an extreme way and that the molten metal
15 be agitated vigorously to keep the ceramic uniformly distributed in the melt due to the
16 difference in density of metal and ceramic.

17 Polymers can be sprayed using the present invention by feeding a molten or
18 plastisized polymer, by in-flight melting of polymer powders fed into the nozzle in
19 aerosol form, or more typically, by dissolving the polymer in an appropriate solvent and
20 spraying the solution. High temperature gas facilitates in-flight evaporation of the
21 solvent from the atomized droplets, and the remainder of the solvent is evaporated at the

1 pattern. As with metals, polymers can also be codeposited with ceramics to form
2 polymer matrix composites.

3 The nozzle/feed assembly is designed to produce sprays of very fine droplets
4 having a narrow size distribution. These conditions offer the greatest flexibility for
5 controlling droplet temperature, momentum and flow pattern, as well as the resultant
6 microstructure of the deposit. FIG. 3 shows an alternate embodiment of the present
7 invention and differs from the device shown in FIG. 1 in that the liquid orifice(s) (i.e., the
8 orifices through which the liquid flows before entering the flow channel of the nozzle),
9 are located in the diverging section of the nozzle near the exit of the nozzle. In contrast,
10 in FIG. 1, the orifices are located upstream of the nozzle's throat. In the devices shown in
11 FIG. 1 and FIG. 3 liquid enters the flow channel through tubes 38 which terminate near
12 the longitudinal axis of the flow channel of the nozzle where the gas velocity is generally
13 highest. This provides the greatest dynamic pressure for atomization of the liquid and
14 often times provides the most finely atomized droplets. Furthermore, by feeding the
15 liquid proximate to the flow channel longitudinal axis, the present invention eliminates
16 the disadvantage of conventional spray forming techniques of agglomeration of the
17 atomized droplets on the side walls of the flow channel. The agglomeration of droplets
18 on the side walls of the flow channel results in larger diameter droplets being directed
19 toward the pattern. To further ameliorate this situation, an alternate embodiment of the
20 present invention is the feeding of the liquid into the flow channel near the flow channel
21 outlet. Spray nozzles have been designed, constructed and operated with the liquid
22 orifices located at various locations along the length of flow channel and at various

1 locations within the flow channel of the nozzle. Moreover, nozzles have been designed,
2 constructed, and operated which utilize a single slit-shaped liquid orifice or a set of tubes
3 that span the width of the nozzle. Therefore, FIGs. 1 and 2 are provided as two examples,
4 without limiting the scope of the technique.

5 The extent of in-flight cooling of the atomized droplets prior to impacting the
6 pattern depends upon the superheat of the liquid, the droplet size, the atomizing gas
7 temperature, the thermal conductivity and thermal diffusivity of the atomizing gas, the
8 nozzle-to-pattern distance, the temperature and thermal properties of the quench gas, (i.e.,
9 the gas which is entrained into the spray plume outside the nozzle), and other factors.

10 FIG. 4 is a graph illustrating the influence the quench gas has on cooling the gas jet after
11 it exits the nozzle. The data shown in FIG. 4 was generated by flowing high temperature
12 (about 500 °C) argon gas through a spray nozzle at various nozzle inlet pressures ranging
13 from 137 kPa (20 psia) to 165 kPa (24 psia). The temperature of the gas jet after it exits
14 the nozzle is plotted against distance from the nozzle's exit plane. Room temperature
15 argon gas was entrained into the jet causing the temperature of the gas in the jet to
16 decrease with increasing distance from the nozzle. This cooling effect provides a heat
17 sink for cooling atomized droplets, thereby allowing undercooled and partially solidified
18 droplets to be formed in flight. FIGs 4A, 4B and 4C show the geometrical parameters
19 (FIG. 4A) and experimental data (FIG.s 4B and 4C) used to generate the curves of FIG. 4.
20 Seven thermocouples (TC#1 through TC#7) were spaced in the gas jet down stream of
21 the exit of the nozzle at the distances shown in FIG. 4B.

FIG. 5 shows the nozzle assembly of the present invention contained within a nozzle chamber 50 and a spray chamber 51 in which the atomized droplets are directed toward the pattern. By controlling the temperature, pressure and composition of the quench gas contained within the spray chamber 51, the present invention is capable of finely controlling the cooling rate of the atomized droplets prior to the droplets impacting upon the pattern. Low temperature quench gas provides rapid cooling of droplets, while preheated quench gas reduces the cooling rate of the droplets. Quench gas may consist of cryogenic gas (and liquid) tapped directly off a liquid nitrogen tank to rapidly quench the spray plume. In other experiments, cryogenically cooled helium gas served as the quench gas. Alternatively, inert gas (e.g., argon, helium, etc.) at room temperature or warmed to less than 500° C has been used as the quench gas. The spray chamber 51 also may provide for an observation window 40 and rupture disk 44. Pattern induction furnace may be provided to control the temperature of the pattern on which the atomized droplets are deposited.

For a better understanding of the present invention, the following examples are provided to illustrate the spray forming technique.

Experimental Studies

Bench-scale nozzles having transverse throat widths of 17 mm were typically operated at gas-to-metal mass ratios (for tool steel) of approximately 1, with metal throughputs of about 4 Kg/s per meter of nozzle throat width.

In one study, a metal mold weighing 5 Kg was produced in about 3 minutes by spray forming P-20 tool steel onto a ceramic (alumina) pattern having a complex shape.

1 Replication of surface features, including fine scratches in the pattern, was excellent. The
2 mechanical properties of the mold (strength, hardness, etc.) were comparable to those of a
3 mold machined from commercial forced prehardened material and the mold was found to
4 produce a comparable number of plastic injection molded parts.

5 Bench-scale nozzles having transverse throat widths of 17 mm were typically
6 operated at gas-to-metal mass ratios (for tin) of approximately 10, with metal throughputs
7 of about 500 g/s per meter of nozzle throat width.

8 In one study, a metal mold weighing 250 grams was produced in about 5 minutes
9 by spray forming tin onto a low-density polyethylene pattern having a complex shape.
10 The pattern was not damaged despite the fact that the temperature of the molten metal
11 within the reservoir was 300 °C, which greatly exceeded the melting point of the pattern
12 (~100 °C). Replication of surface features, including fine scratches in the pattern, was
13 excellent. The surface of the mold at the deposit/pattern interface was mirror-like
14 indicating that peak-to-valley surface roughness was likely less than about 26
15 nanometers. Patterns of a variety of other plastics, including, poly(methyl methacrylate),
16 polycarbonate, polyvinyl chloride and polystyrene have also given good results, as have
17 advanced high temperature polymers such as polyimide and polyetherimide.

18 The as-deposited grain structure observed in this experimental study was equiaxed
19 with a fairly narrow range of fine (~6 to 15 μm) grain sizes -- much finer than the
20 massive grains found in conventional cast objects. As-deposited density, measured by
21 water displacement using Archimedes' principle, was typically in the range of 88 to 97%
22 of theoretical depending upon spray conditions.

1 The molten metal used to produce the deposit was very finely atomized.
2 Unconsolidated powder was collected and analyzed by wet and dry sieving through fine
3 mesh screens of 300, 250, 210, 150, 125, 90, 75, 63, 53, 38, 25, 18, 15, 10 and 5 μm .
4 Few particles larger than 125 μm were observed. FIG. 6 is a histogram plot that gives the
5 count frequency distribution versus powder size. The ordinate gives the count frequency
6 normalized for the sieve size range, expressed as a percentage of the total counts. The
7 plot indicates that about 85% of the powder particles were $<5 \mu\text{m}$ in diameter. The
8 average particle size was calculated to be 4 μm . FIG. 7 shows a histogram plot that
9 relates mass frequency to powder size for the same tin powder sample, again normalized
10 for the size range of the sieves. When compared with FIG. 6, this distribution reflects the
11 significance of the mass weighting factors (which go as d^3 , where d is the diameter of the
12 powder particle) imposed by relatively small numbers of more massive particles. The
13 mass median diameter, volume mean diameter, and Sauter mean diameter of the powder
14 were, 23 μm , 31.3 μm , and 23.2 μm . The geometric standard deviation was 1.5,
15 indicating a narrow droplet size distribution in the spray plume. SEM analysis indicated
16 that nearly all the particles were spherical. Similar spray conditions were used to spray
17 form a semispherical tin shell using an inflated party balloon as the pattern without
18 bursting the balloon.

19 As another example, GMR 311, a forming-die (Kirksite) alloy having the nominal
20 composition 3% Al, 11% Cu, Zn bal., was spray formed into a complex shape using a
21 poly (methyl methacrylate) (i.e., LuciteTM and PlexiglassTM) pattern. The alloy was
22 superheated to 600 °C and deposited onto the pattern, which has a melting point of about

80 °C, to form a free-standing mold which again replicated the surface features of the pattern extremely well without damaging the pattern. Cold helium and nitrogen have been used as quench gases, as well as room temperature argon. The spray-formed mold weighed about 700 grams and was formed in about ten minutes. Complex molds of this material have also been spray formed using low-density polyethylene patterns such as children's sand toys. The zinc-based die-casting alloy, alloy 3 (Zn, 4% Al), has also been spray formed to form complex free-standing molds using low density polyethylene patterns.

Other high melting point alloys have successfully been spray formed to produce free-standing tooling using the apparatus and methods of the present invention with excellent surface features and shape replication. As-deposited photomicrographs of a sectioned low carbon steel (SAE 1008) sample deposited using the present invention, show that the grain structure is near-equiaxed ferrite, with an average grain size of 16 μm . This highly refined as-deposited average grain size is similar to that found for commercial low-carbon steel hot band. The spray nozzle operated at a static pressure of 206 kPa (30 psia) absolute, measured at the nozzle's inlet. Under single-phase flow conditions, the gas flow field was mapped out using small pitot tube probes. Results indicated that this driving pressure generated supersonic flow conditions with the shock front located in the diverging section near the metal feed location. Gas-to-metal mass ratios were typically about 10. Gas and droplet temperature fell rapidly after exiting the nozzle as the spray plume entrained cool argon. Gas and droplet velocity decreased after exiting the nozzle with larger droplets responding less to drag effects by virtue of their

1 greater momentum. The steel was induction heated to about 1600 °C and atomized using
2 argon or other inert gas heated to about 1000 °C. As-deposited density of the tool,
3 measure by water displacement using Archimedes' principle, was in the range of 88 to
4 97% of theoretical density, with 96% being typical.

5 The ultimate tensile strength of a sectioned aluminum alloy 6061 tool produced
6 by the system of the present invention was measured to be 166 MPa (24 ksi) which is
7 about a 33% improvement in ultimate tensile strength over the wrought, annealed
8 commercial material. This improvement in strength is presumably due to grain structure
9 refinement. This material has been successfully spray deposited onto a variety of pattern
10 materials, including common glass, located about 20 inches from the exit of the nozzle.
11 Argon gas was used as the atomizing gas, and the quench gas was maintained at or near
12 room temperature. Metal mass throughputs were typically 185 g/s per meter of nozzle
13 throat width. The liquid metal was heated about 100 °C above its liquidus temperature
14 and the atomizing gas was heated to about 700 °C. The spray nozzle operated at a
15 pressure of about 206 kPa (30 psia) absolute, measured at the nozzle's inlet.

16 An unetched, polished photomicrograph of a sectioned particulate reinforced
17 metal matrix composite tool produced using the system of the present invention revealed
18 a uniform distribution of silicon carbide particles embedded in an aluminum alloy 6061
19 matrix. Particulate volume fractions have ranged from 4 to 15% as determined by acid
20 dissolution of the matrix, for various spray forming experiments. Higher or lower
21 volume fraction are possible. The composites were produced using matrix spray
22 conditions similar to those described in the preceding paragraph. The ~13 μm SiC

1 particulate was codeposited with the matrix material by injecting an Ar/SiC aerosol into
2 the nozzle upstream of the entry location of the liquid aluminum. The particulate entered
3 the nozzle at or near room temperature, but was quickly heated by the atomizing gas to
4 the desired temperature. Independent temperature control of the metal and particulate
5 phases allows flexibility for controlling the extent of matrix/particulate wetting and
6 interfacial reactions.

7 A linear polyphosphazene polymer (poly[bis(phenoxy)phosphazene] (PPOP))
8 deposit was formed using the system of the present invention. The polymer deposit was
9 formed by depositing atomized droplets of linear PPOP dissolved in tetrahydrofuran
10 (THF) onto patterns of glass and other materials. The spray was generated using a linear
11 converging-diverging (de Laval) geometry nozzle machined from commercial boron
12 nitride rod. Seven percent (by weight) solution of linear PPOP in THF was sprayed. The
13 weight average molecular weight of the polymer was measured to be about 750,000 amu
14 by gel permeation chromatography. Five percent and three percent solution having a
15 polymer weight average molecular weight exceeding one million amu were also sprayed
16 but were found to give less satisfactory results. The solution was warmed to ~45 °C to
17 lower its viscosity and poured into the tundish of the nozzle operating at a static pressure
18 of 137 kPa (20 psia). The solution was aspirated through six small orifices that spanned
19 the width of the nozzle. Solution throughput was about 0.4 Kg/second per meter of
20 nozzle throat width. The corresponding gas-to-polymer solution mass ratio was about 4.
21 The solution was sheared and atomized, resulting in very fine droplets that were entrained
22 by the gas stream and transported to a moving pattern. Solvent molecules were shed from

1 the atomized particles during their flight, and the remainder of the solvent evaporated at
2 the substrate. While control of atomizing gas temperature provided a convenient vehicle
3 for adjusting the evaporation rate of the solvent, room temperature argon was used
4 because the equilibrium vapor pressure of THF (147 torr at 20 °C) was high enough to
5 allow facile evaporation of the solvent. Upon impacting the substrate, individual polymer
6 molecules within adjacent droplets interwove while shedding any remaining solvent. The
7 resultant polymer deposit appeared coherent and uniform. A SEM analysis of the deposit
8 revealed that the deposit at the deposit/pattern interface was specular (i.e., it reflected
9 light and replicated surface features on the pattern very well). The deposit surface away
10 from this interface, however, was matte.

11 The foregoing description of a preferred embodiment of the invention has been
12 presented for purposes of illustration and description. It is not intended to be exhaustive
13 or to limit the invention to the precise form disclosed, and obviously many modifications
14 and variations are possible in light of the above teaching. The embodiments described
15 explain the principles of the invention and practical application and enable others skilled
16 in the art to utilize the invention in various embodiments and with various modifications
17 as are suited to the particular use contemplated. It is intended that the scope of the
18 invention be defined by the claims appended hereto.

WE CLAIM:

1 1. A system for the spray forming manufacture of near net shape molds, dies
2 and related toolings, comprising:

3 a nozzle having a flow channel, said flow channel having an inlet end, an outlet
4 end and a longitudinal axis;

5 a liquid reservoir in fluid communication with said nozzle flow channel, said
6 reservoir containing a liquid material capable of forming a mold, said liquid being
7 pressurized in a pressurized reservoir and injected from said reservoir through a conduit
8 ending in said nozzle flow channel between said inlet and outlet ends and proximate to
9 said nozzle longitudinal axis;

10 means for flowing a high temperature atomizing gas at a flow velocity ranging
11 from high subsonic through supersonic velocities through the nozzle flow channel from
12 the inlet end to the outlet end to atomize the liquid injected into the flow channel into a
13 plume of atomized droplets directed to a chamber containing a quench gas, said quench
14 gas having a controlled temperature and composition for controlling the in-flight cooling
15 of the atomized droplets;

16 means for directing and depositing the cooled atomized droplets onto a pattern to
17 form the mold.

1 2. The system of claim 1 wherein said quench gas is selected from a group
2 consisting of nitrogen, helium, argon, oxygen, air, and combinations thereof.

3 3. The system of claim 1 further comprising means for independently heating the
4 nozzle and reservoir.

1 4. The system of claim 1 further comprising means for providing relative
movement between nozzle and the pattern.

1 5. The system of claim 1 wherein a plurality of liquid materials capable of
2 forming a mold are injected separately into the nozzle flow channel.

1 6. The system of claim 1 wherein the nozzle flow channel converges to a choke
2 portion located between the inlet end and the outlet end, and diverges between the choke
portion and the outlet end.

1 7. The system of claim 1 wherein the liquid material is injected into the nozzle
2 flow channel proximate to the longitudinal axis between the inlet end and the choke
3 portion of the flow channel.

1 8. The system of claim 1 wherein the liquid material is injected into the nozzle
2 flow channel proximate to the longitudinal axis between the choke portion and the outlet
3 end of the flow channel.

1 9. The system of claim 1 wherein the liquid material is a molten metal.

2 10. The system of claim 1 wherein the liquid material is a molten metal
3 containing solid particles.

1 11. The system of claim 10 wherein the molten metal is selected from the group
2 consisting of tin, aluminum, zinc, and copper.

1 12. The system of claim 1 wherein the liquid material is a molten metallic alloy.

1 13. The system of claim 12 wherein the molten metallic alloy is selected from the
2 group consisting of steel, bronze and brass.

1 14. The system of claim 1 wherein the liquid material is a polymer solution.

1 15. The system of claim 1 wherein the liquid material is a polymer solution
2 containing solid particles.

1 16. The system of claim 1 wherein the means for injecting the liquid material into
2 the nozzle flow channel is accomplished by pressurizing the liquid reservoir.

1 17. The system of claim 1 wherein the nozzle flow channel has a linear transverse
2 cross-sectional geometry.

1 18. A system for the spray forming manufacture of near net shape molds, dies
2 and related toolings, comprising:

3 a plurality of nozzles, each nozzle having a flow channel, each of said flow
4 channels having an inlet end, an outlet end and a longitudinal axis;

5 a liquid reservoir in fluid communication with each of said nozzle flow channels,
6 said reservoir containing a liquid material capable of forming a mold, said liquid being
7 pressurized in a pressurized reservoir and injected from said reservoir through a conduit
8 ending in said nozzle flow channel between said inlet and outlet ends and proximate to
9 said nozzle longitudinal axis;

10 a high temperature atomizing gas at a flow velocity ranging from high subsonic
11 through supersonic velocities through each of the nozzle flow channels from the inlet end
12 to the outlet end to atomize the liquid injected into the flow channels into a plume of
13 atomized droplets directed to a chamber containing a quench gas, said quench gas having
14 a controlled temperature and composition for controlling the in-flight cooling of the
15 atomized droplets;

16 means for directing and depositing the cooled atomized droplets onto a pattern to
17 form the mold.

1 19. The system of claim 18 further comprising means for independently heating
2 the nozzles and reservoirs.

1 20. The system of claim 18 further comprising means for providing relative
2 movement between nozzle and the pattern.

1 21. The system of claim 18 wherein a plurality of liquid materials capable of
2 forming a mold are injected separately into the nozzle flow channel.

1 22. The system of claim 18 wherein the nozzle flow channel converges to a choke
2 portion located between the inlet end and the outlet end, and diverges between the choke
3 portion and the outlet end.

1 23. The system of claim 22 wherein the liquid material is injected into the nozzle
2 flow channel proximate to the longitudinal axis between the inlet end and the choke
3 portion of the flow channel.

1 24. The system of claim 22 wherein the liquid material is injected into the nozzle
2 flow channel proximate to the longitudinal axis between the choke portion and the outlet
3 end of the flow channel.

1 25. The system of claim 18 wherein the liquid material is a molten metal.

1 26. The system of claim 18 wherein the liquid material is a molten metal
2 containing solid particles.

3 27. The system of claim 26 wherein the molten metal is selected from the group
4 consisting of tin, aluminum, zinc, and copper.

1 28. The system of claim 18 wherein the liquid material is a molten metallic alloy.

1 29. The system of claim 28 wherein the molten metallic alloy is selected from the
2 group consisting of steel, bronze and brass.

1 30. The system of claim 18 wherein the liquid material is a polymer solution.

1 31. The system of claim 18 wherein the liquid material is a polymer solution
2 containing solid particles.

1 32. The system of claim 18 wherein the means for injecting the liquid material
2 into each of the nozzle flow channels is accomplished by pressurizing the liquid reservoir.

1 33. The system of claim 18 wherein each of the nozzle flow channels has a linear
2 transverse cross-sectional geometry.

1 34. A system for the spray forming manufacture of near net shape molds, dies
2 and related toolings, comprising:

3 a nozzle having a flow channel, said flow channel having an inlet end, an outlet
4 end, and a longitudinal axis;

5 a plurality of reservoirs in separate fluid communication with said nozzle flow
6 channel, at least one of said reservoirs containing a liquid material capable of forming a
7 mold, said liquid being pressurized in a pressurized reservoir and injected from said
8 reservoir through a conduit ending in said nozzle flow channel between said inlet and
9 outlet ends and proximate to said nozzle longitudinal axis;

10 means for flowing a high temperature atomizing gas at a flow velocity ranging
11 from high subsonic through supersonic velocities through the nozzle flow channel from
12 the inlet end to the outlet end to atomize the liquid injected into the flow channel into a
13 plume of atomized droplets directed to a chamber containing a quench gas, said quench
14 gas having a controlled temperature and composition for controlling the in-flight cooling
15 of the atomized droplets;

16 means for directing and depositing the cooled atomized droplets onto a pattern to
17 form the mold.

1 35. The system of claim 34 wherein at least one of said plurality of reservoirs
2 contains solid particles, said solid particles being injected into said nozzle flow channel
3 between said inlet and outlet ends and proximate to said flow channel longitudinal axis,
4 said injected solid particles thereby mixing with the injected liquid materials and
5 codeposited onto a pattern to form the mold.

ABSTRACT

1 A system for the spray forming manufacturing of near-net-shape molds, dies and
2 related toolings, wherein liquid material such as molten metal, metallic alloys, or
3 polymers are atomized into fine droplets by a high temperature, high velocity gas and
4 deposited onto a pattern. Quenching of the in-flight atomized droplets provides a heat
5 sink, thereby allowing undercooled and partially solidified droplets to be formed in-flight.
6 Composites can be formed by combining the atomized droplets with solid particles such
7 as powders, whiskers or fibers.

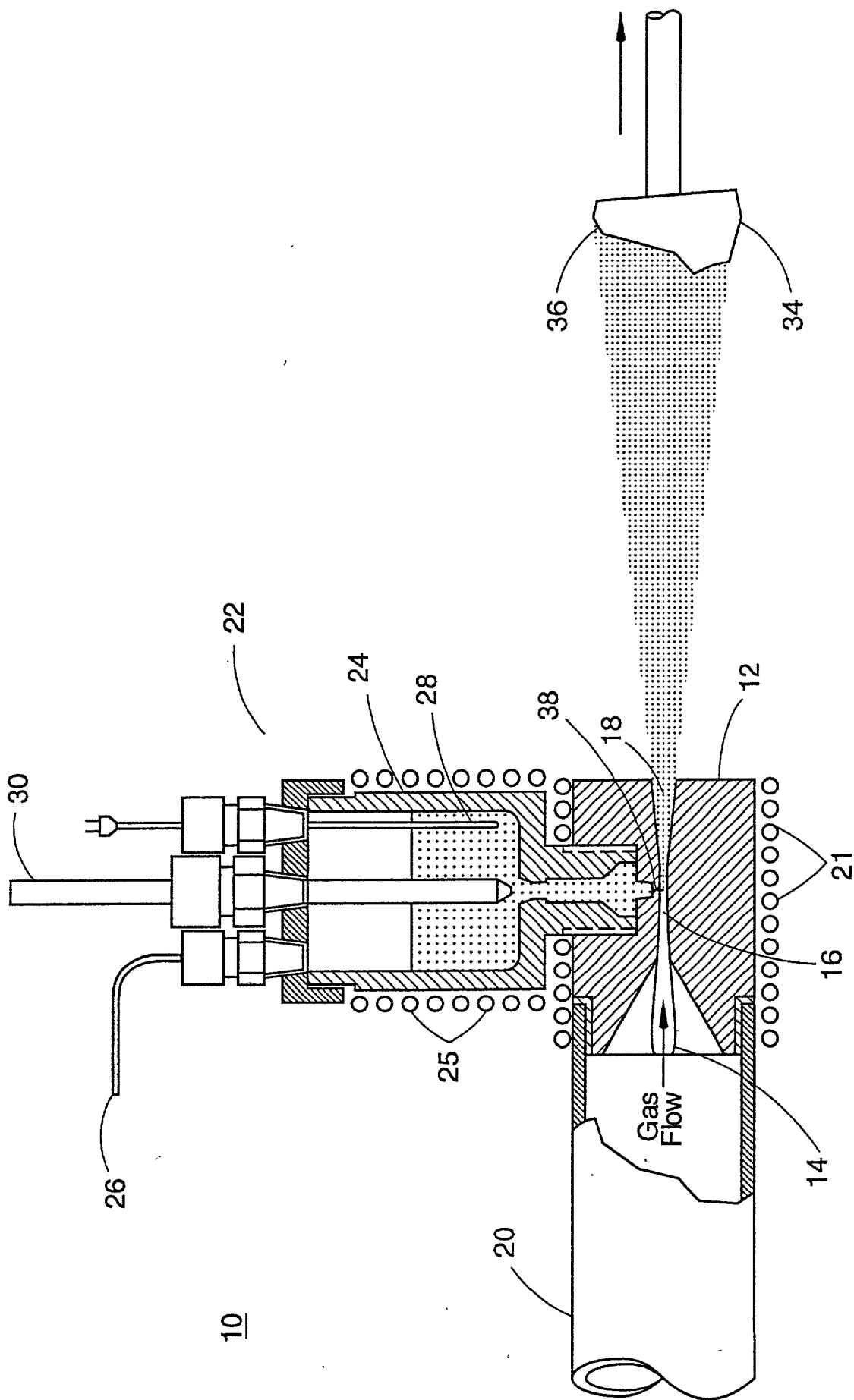


Fig. 1

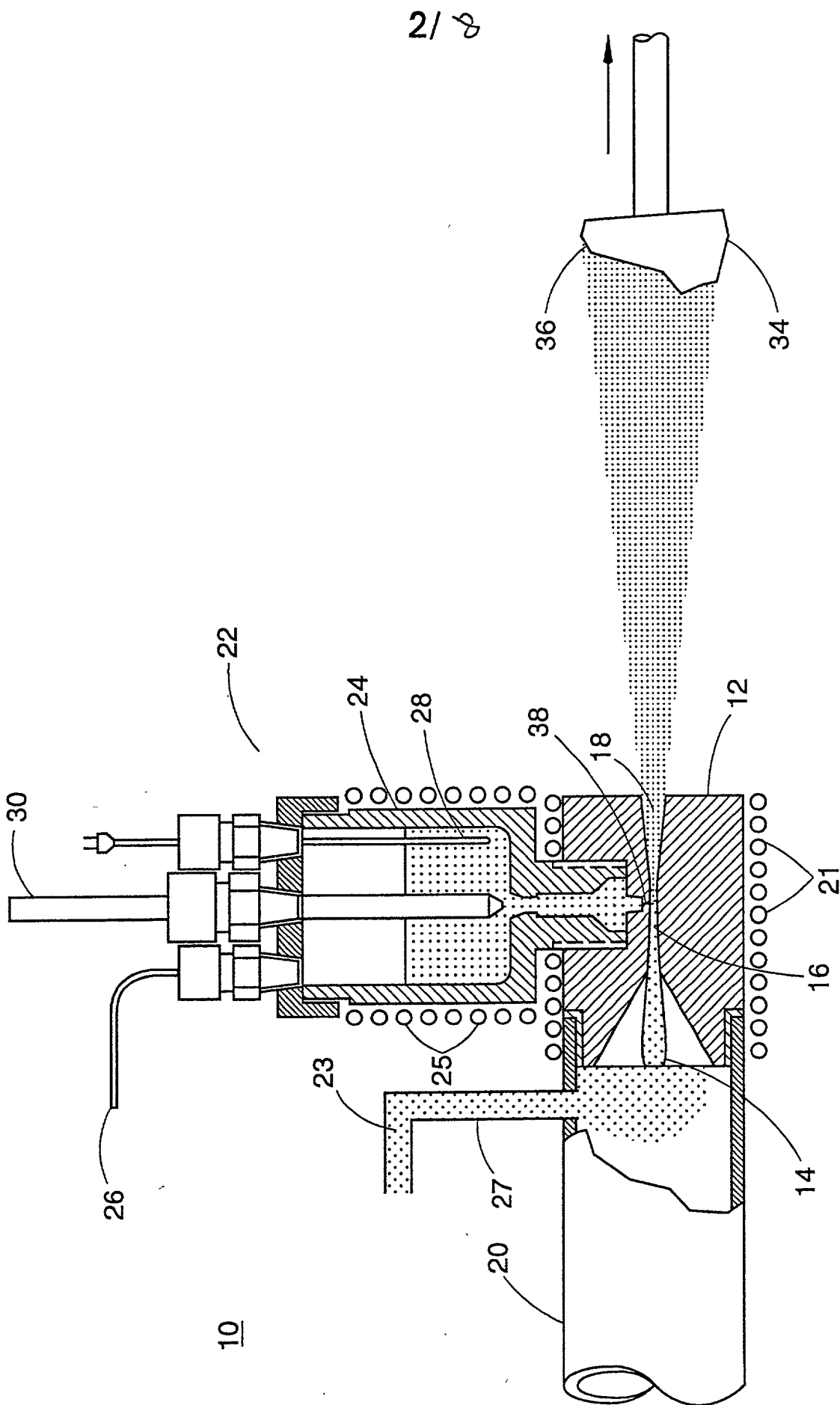
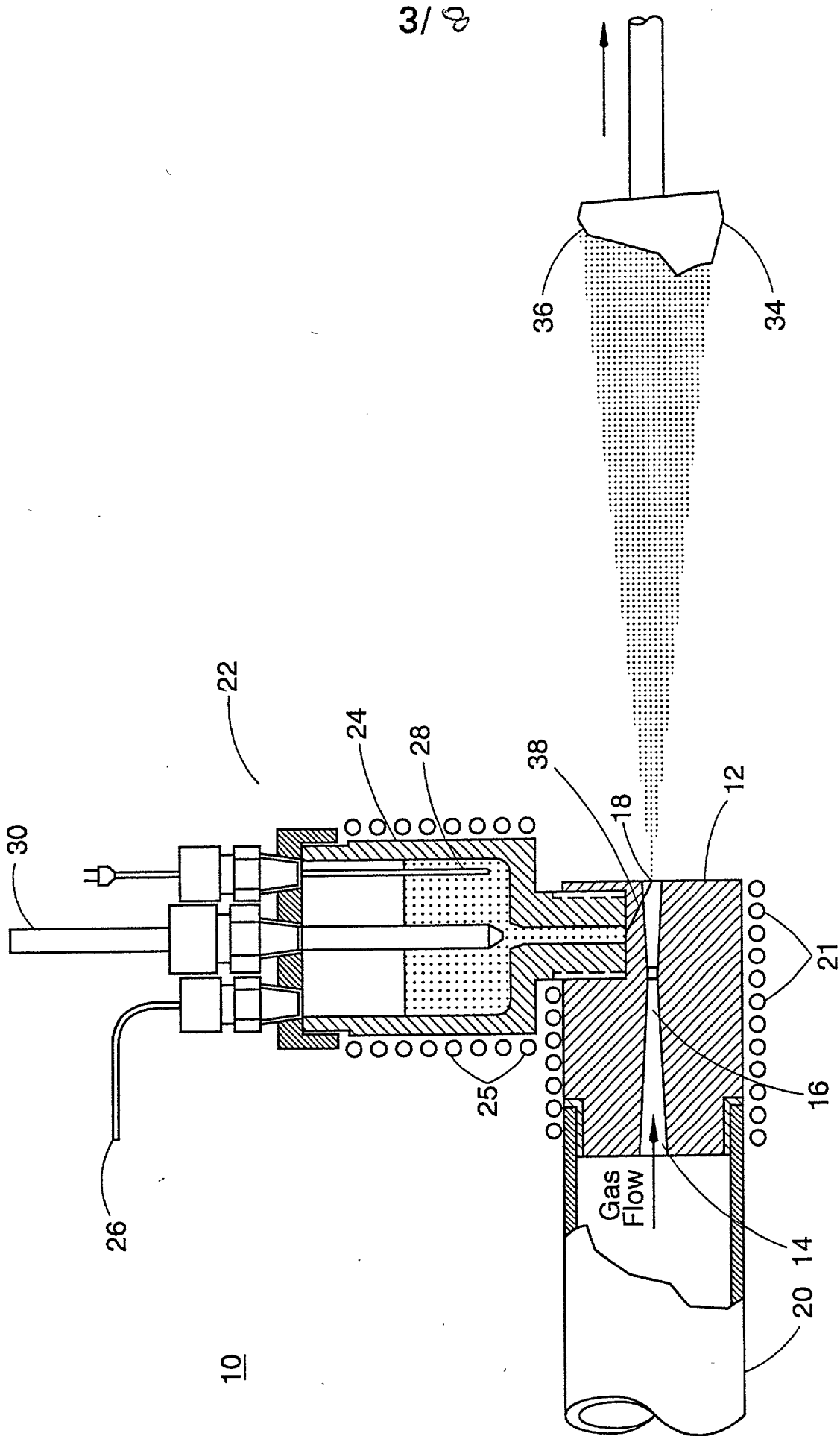


Fig. 2



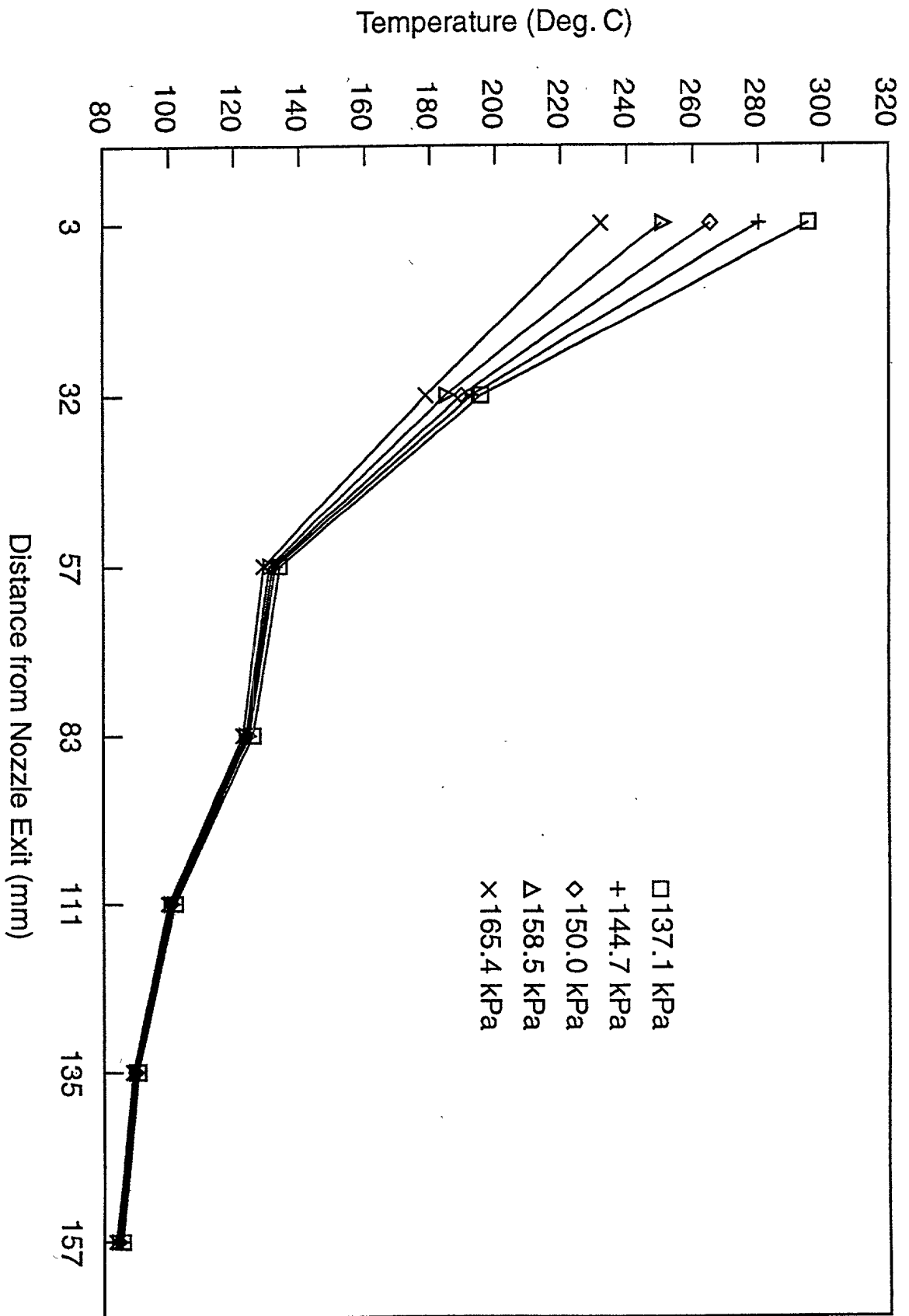


Fig. 4

Nozzle Information

• Nozzle Information:	14.0°
• Exit Angle	14.0°
• Distance from Liquid Orifice to Nozzle Exit (inches)	1.018
• Number of Orifices	6.0
• Orifice Area (square inches)	0.000314
• Total Area of Liquid Orifices (square inches)	0.0019
• Cross Sectional Area of Nozzle Throat (square inches)	0.06
• Cross Sectional Area of Gas Stream at Nozzle Exit (square inches)	0.266

Fig. 4A

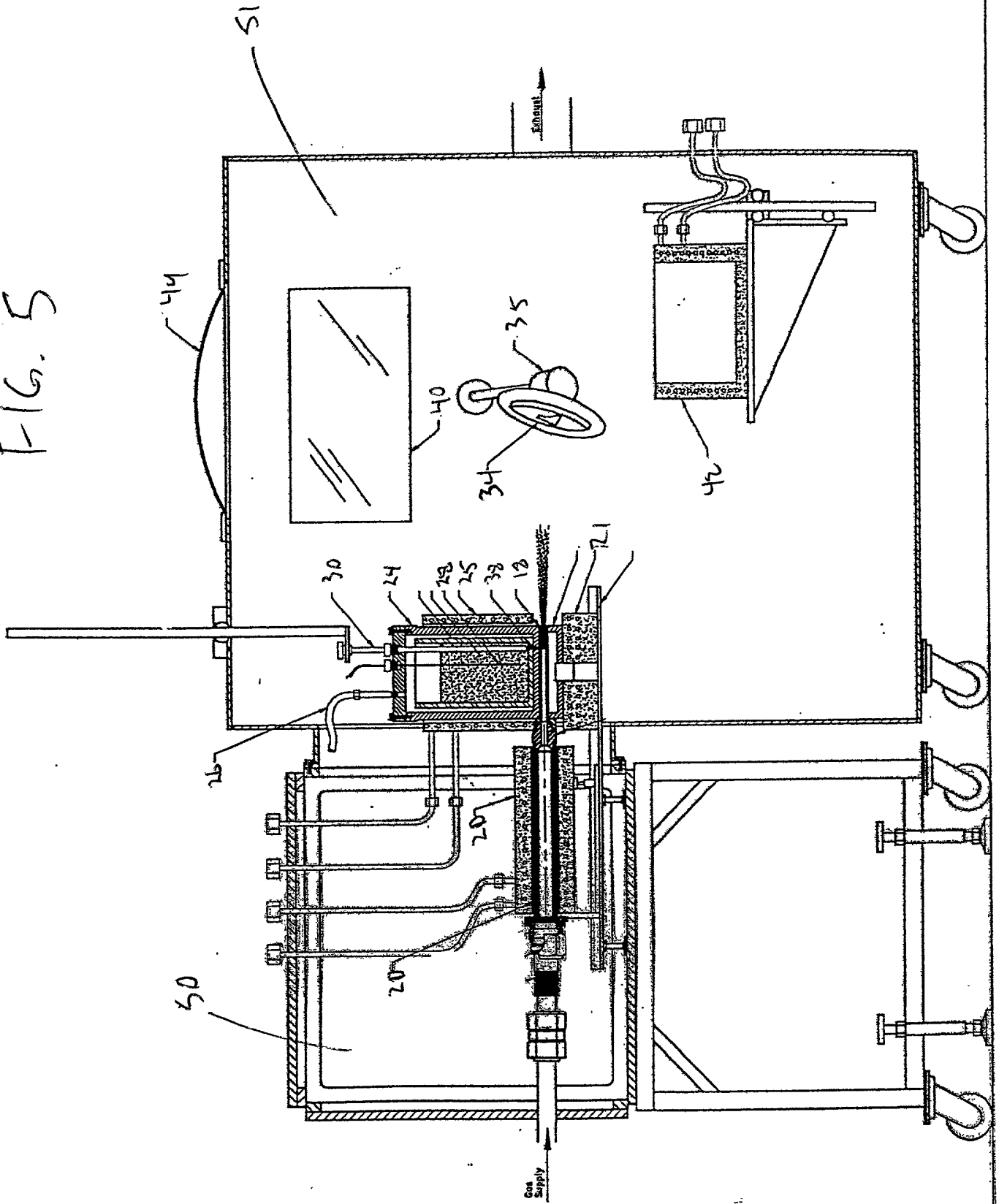
Run Time (sec)	TC #1 (°C)	TC #2 (°C)	TC #3 (°C)	TC #4 (°C)	TC #5 (°C)	TC #6 (°C)	Argon TC #7 (°C)	Gas Flow (slpm)
45.5	309.7	165.3	107.7	100.6	86.0	79.5	74.8	253.7
105.5	318.8	190.5	122.6	113.5	92.9	83.9	79.1	283.6
165.5	318.0	199.0	129.8	120.1	97.3	87.0	81.6	305.8
215.5	324.6	201.3	134.5	124.8	101.0	90.0	83.9	329.5
285.5	311.7	200.0	136.0	127.0	102.5	91.1	85.2	355.9
345.5	295.9	196.6	135.3	127.0	102.5	90.6	84.6	381.2
405.5	279.9	194.4	135.1	127.2	102.9	91.2	85.1	412.2
465.5	266.9	190.6	133.4	126.2	101.9	90.6	84.1	439.3
525.5	251.8	186.0	131.9	125.4	101.4	90.1	84.2	474.7
585.5	233.4	180.1	130.3	123.8	100.4	89.5	83.7	504.5
Distance from Nozzle Exit (inches)								
	0.125	1.25	2.25	3.25	4.375	5.312	6.187	

Fig. 4B

Gas Temperature Nozzle Inlet (°C)	Nozzle Temperature Liquid Orifice (°C)	Chamber Temperature (°C)	Nozzle Inlet Pressure (psia)
552.7	347.9	38.0	15.096
555.8	356.7	39.0	16.168
557.2	362.7	39.7	17.074
548.5	365.0	40.0	18.020
527.3	364.1	41.1	19.003
501.7	359.3	41.9	19.926
476.0	350.9	42.0	20.982
453.9	340.9	43.4	21.928
429.2	329.3	44.0	23.054
409.0	317.4	44.1	23.968

Fig. 4B

FIG. 5



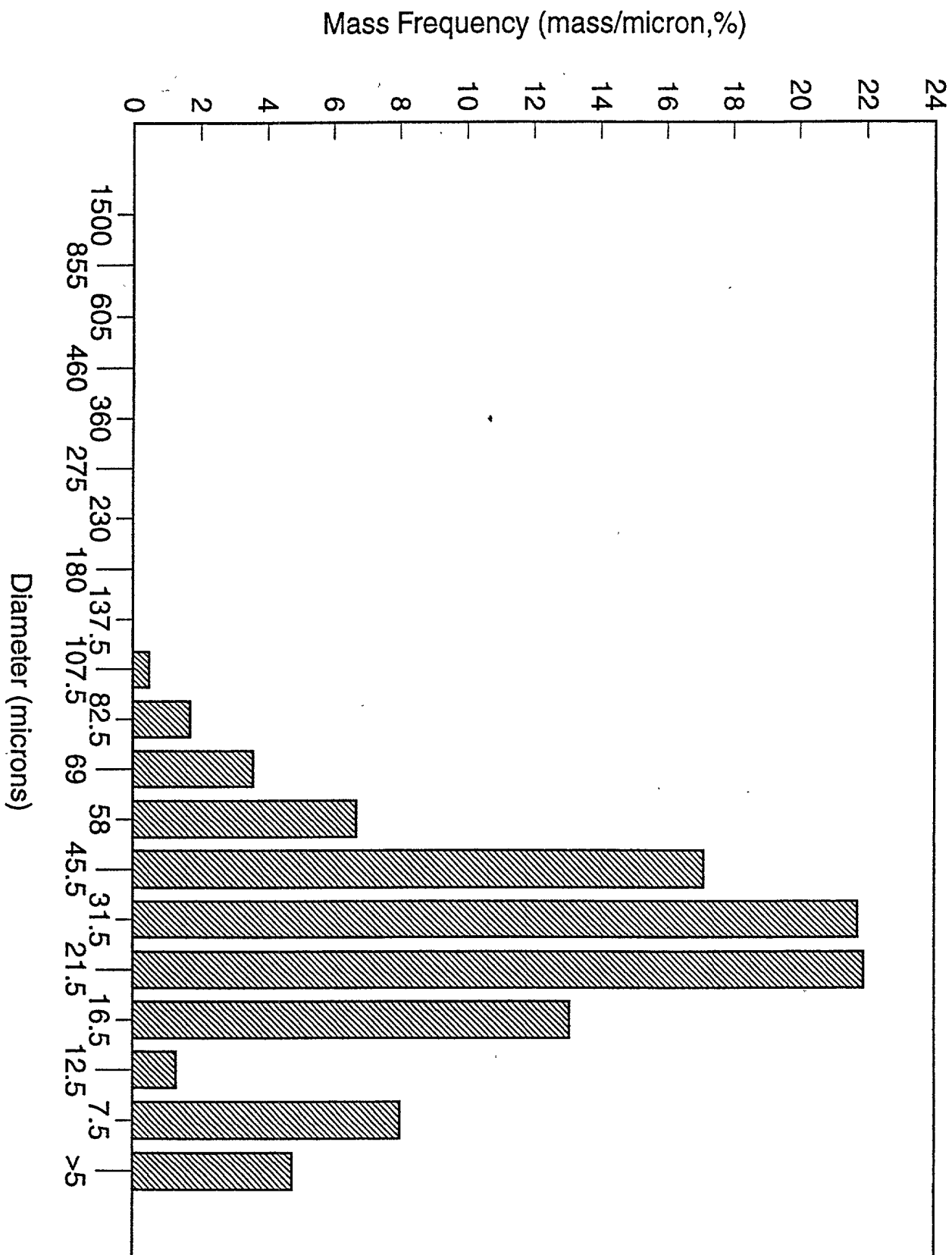


Fig. 7

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DECLARATION FOR UTILITY OR DESIGN PATENT APPLICATION (37 CFR 1.63)	Attorney Docket Number	EGG-PI-612A1a
	First Named Inventor	Kevin M. McHugh
	COMPLETE IF KNOWN	
	Application Number	/
	Filing Date	
	Group Art Unit	
<input checked="" type="checkbox"/> Declaration Submitted with Initial Filing	OR	<input type="checkbox"/> Declaration Submitted after Initial Filing (surcharge (37 CFR 1.16 (e)) required)
Examiner Name		

As a below named inventor, I hereby declare that:

My residence, post office address, and citizenship are as stated below next to my name.

I believe I am the original, first and sole inventor (if only one name is listed below) or an original, first and joint inventor (if plural names are listed below) of the subject matter which is claimed and for which a patent is sought on the invention entitled

Rapid Solidification Processing System for Producing Molds, Dies and Related Tooling

the specification of which ☒ is attached hereto OR ☐ was filed on (MM/DD/YYYY) as United States Application Number or PCT International Application Number and was amended on (MM/DD/YYYY) (if applicable)

I hereby state that I have reviewed and understand the contents of the above identified specification, including the claims, as amended by any amendment specifically referred to above.

I acknowledge the duty to disclose information which is material to patentability as defined in 37 CFR 1.56.

I hereby claim foreign priority benefits under 35 U.S.C. 119(a)-(d) or 365(b) of any foreign application(s) for patent or inventor's certificate, or 365(a) of any PCT international application which designated at least one country other than the United States of America, listed below and have also identified below, by checking the box, any foreign application for patent or inventor's certificate, or of any PCT international application having a filing date before that of the application on which priority is claimed

Prior Foreign Application Number(s)	Country	Foreign Filing Date (MM/DD/YYYY)	Priority Not Claimed	Certified Copy Attached?	
				YES	NO
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☐ Additional foreign application numbers are listed on a supplemental priority data sheet PTO/SB/02B attached hereto:

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[Page 1 of 2]

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U.S. Parent Application or PCT Parent Number	Parent Filing Date (MM/DD/YYYY)	Parent Patent Number (if applicable)
07/983,459	11/30/92	
08/320,032	10/07/94	5718863
09/023,037	02/13/98	

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Given Name (first and middle (if any))		Family Name or Surname			
Kevin M.		McHugh			
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